

# Transition from isothermal to chain-thermal flame-propagation regimes in the branching-chain decomposition of nitrogen trichloride

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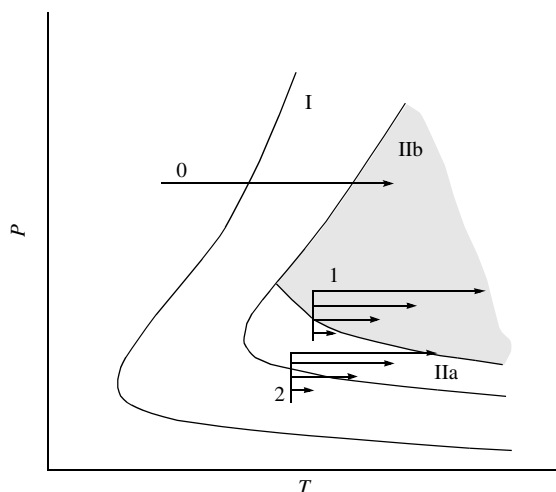
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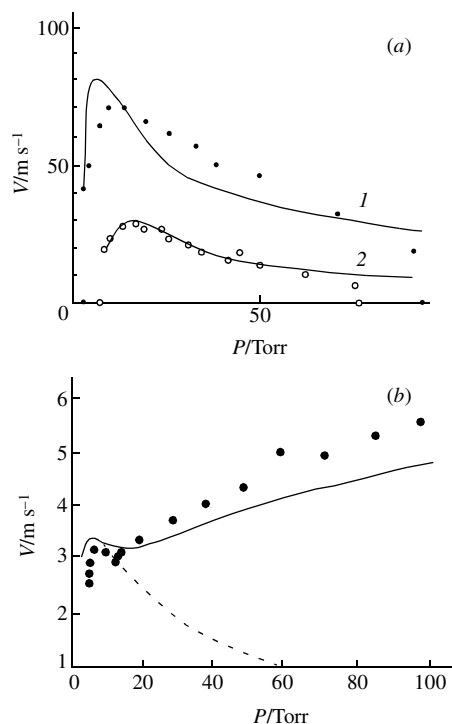
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The title transition has been detected in a mixture of nitrogen trichloride (4%) with helium. The occurrence of a non-linear branching step in the branched-chain reaction shortens the time interval of the development of a chain-thermal flame.

Two general types of the propagation of subsonic flames are known in the theory of combustion: an isothermal regime and a thermal<sup>1</sup> (or, more precisely, chain-thermal) regime. The velocity of isothermal flames is determined by the diffusion of the active centres (atoms and radicals) of a branched-chain reaction (BCR) into an unreacted mixture.<sup>1</sup> The BCR mechanism must include non-linear chain branching (in this reaction, an increase in the number of free valences is due to the interaction of active centres).<sup>2,3</sup> The area of isothermal flame propagation (IFP) (I in Figure 1) is broader than self-ignition area II. The structure of the ignition area in BCR (a pressure–temperature plot) is shown in Figure 1. Chain-thermal flame propagation (CTFP), as distinct from IFP, is due to heat evolution in the front of a developing BCR. The non-Arrhenius dependence<sup>5</sup> of the branching on temperature is the positive feedback, which provides the occurrence of the stationary front of combustion. Chain-thermal flames have been widely investigated in BCR, including only linear branching.<sup>4,6,7</sup> The self-ignition area of these linear BCR II includes isothermal area IIa and chain-thermal explosion area IIb, which corresponds both to developing chain avalanche and accelerating heat accumulation.<sup>4</sup> The stationary flame propagation in linear BCR in the vicinity of the lower self-ignition limit (IIa) is ruled out because the warming-up is missing. At pressures close to the lower boundary of IIa, the warming-up is reasonably large to warm the nearest layers of an unreacted gas up to the self-ignition temperature (arrows 1 in Figure 1; in this case, the stationary combustion wave, namely CTFP, occurs). Therefore, in order that a stationary flame may develop, linear BCR must be initially in self-ignition area, or the initiating impulse (e.g., a spark) must provide the warming-up that is sufficient to transfer the BCR to the area close to IIb (arrow 0 in Figure 1). However this limitation does not take place for non-linear BCR, in which



**Figure 1** The ignition areas in BCR. (I) IFP area; (IIa) isothermal self-ignition area and (IIb) chain-thermal explosion area. Arrows: (0) initiated ignition in linear BCR; (1) transition of a chain self-ignition to a chain-thermal one (or to CTFP); (2) transition of an isothermal flame propagation to a chain-thermal one. The lengths of the arrows correspond to the warming-up.



**Figure 2** Dependence of the flame propagation velocity on total pressure in the mixtures of  $\text{NCl}_3$  with He. (a) Isothermal flame,<sup>9</sup> (1) points (experiment);  $\text{NCl}_3$ , 0.38%; curve indicates numerical simulation for 0.38%  $\text{NCl}_3$  in He; (2) circles (experiment);  $\text{NCl}_3$ , 0.11%, curve indicates numerical simulation for 0.11%  $\text{NCl}_3$  in He; (b) chain-thermal flame, points (experiment), 4%  $\text{NCl}_3$  in He; curves indicate numerical simulation, solid line:  $Q_1 = 17 \text{ kcal mol}^{-1}$ ,  $Q_2 = 34 \text{ kcal mol}^{-1}$ , dotted line:  $Q_1 = 0$ ,  $Q_2 = 34 \text{ kcal mol}^{-1}$ .

the stationary flame propagation may occur in both areas I and II. In this work, the transition of the flame propagation regime from area I to II (arrows 2 in Figure 2), which is possible only in non-linear BCR, is studied.

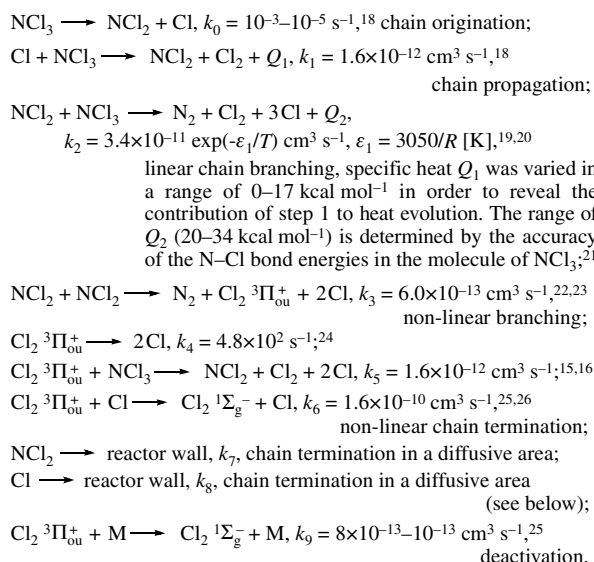
IFP can be observed in dilute mixtures of  $\text{CS}_2$  with  $\text{O}_2$ ,<sup>2,3</sup> thermal decomposition of  $\text{NCl}_3$ ,<sup>8</sup> fluorination of difluoromethane,<sup>9</sup> and oxidation of silane and dichlorosilane.<sup>10,11</sup> Since IFP occurs at very low fuel contents ( $> 0.03\%$ ),<sup>2,3</sup> the interest in IFP is connected directly with explosion safety problems:  $\text{NCl}_3$  is formed in the commercial production of  $\text{Cl}_2$ ,<sup>12</sup> and silanes are widely used in microelectronics.<sup>13</sup> Therefore, a topical problem is to study flame propagation in non-linear BCR, namely the transition from IFP to CTFP. Thermal decomposition of gaseous nitrogen trichloride ( $\text{NCl}_3$ ) is an example of low temperature BCR. The BCR is convenient for attacking the problem because both linear and non-linear chain branching play an important role in this BCR. The kinetics and mechanism of the BCR were considered previously.<sup>8,14–17</sup>

The aim of this work was to detect and study the transition from IFP to CTFP by the example of the decomposition of nitrogen trichloride in a gaseous phase. The regularities obtained

were applied to develop a one-dimensional model of flame propagation.

The experiments were carried out under static conditions at 293 K, total pressures of 2–100 Torr and  $[\text{NCl}_3] = 1\text{--}4\%$ . A cylindrical quartz reactor (80 cm in length and 6 cm in diameter) had inlets for gas evacuation and optical windows. A rapidly heated small furnace placed on the butt end of the reactor provided ignition. After the ignition, a flame propagated into the cool part of the reactor (at 293 K). The velocity of flame travelling was recorded by three photomultiplier tubes equipped with light guides placed 20 cm apart using an oscilloscope. The inner surface of the reactor was covered with magnesium oxide, which provides the diffusive area of chain termination.<sup>8,14</sup> The total pressure was measured with a sensitive pressure gauge ( $10^{-3}$  Torr). The concentration of  $\text{NCl}_3$  in helium was determined from a change in the total pressure after ignition by the stoichiometry of the reaction  $2\text{NCl}_3 \rightarrow \text{N}_2 + 3\text{Cl}_2$ .<sup>17</sup> Liquid  $\text{NCl}_3$  was obtained and gaseous mixtures were prepared by the published procedures.<sup>14</sup> The reactor was evacuated to  $4 \times 10^{-4}$  Torr before each experiment.

It was found<sup>8</sup> that a pressure range in which an isothermal flame propagation occurs [Figure 2(a)] expands with an increase in the  $\text{NCl}_3$  concentration. As this takes place, the flame propagation area expands in such a way that the upper limit of the flame propagation no longer exists over a certain concentration of  $\text{NCl}_3$  in He [Figure 2(b), points]. This means that the role of warming-up markedly increases over certain ranges of total pressures and concentrations of  $\text{NCl}_3$ . Let us consider this phenomenon. The kinetic mechanism of the chemical decomposition of  $\text{NCl}_3$  can be represented as follows:<sup>8,14–17</sup>



It should be noted that the set of reactions (1)–(9) is identical to that considered previously.<sup>15,16</sup> The results<sup>16</sup> of numerical calculations of IFP in dilute mixtures of  $\text{NCl}_3$  with He,  $\text{CO}_2$  and  $\text{Cl}_2$  based on reactions (1)–(9) are in good agreement with experimental data. The reaction of termolecular chain termination is unclear.<sup>18</sup> However, step (9) can explain the occurrence of the upper limit of IFP.<sup>16</sup> Thus, the value of  $k_9$  can be considered only as its upper limit, *i.e.*, both deactivation and termolecular termination are approximated by properly choosing  $k_9$ . As is known, the stationary propagation of a reaction wave must be considered with no regard for a chain origination reaction.<sup>27</sup> The one-dimensional problem was examined. We determine the dimensionless variables and parameters similarly to ref. 16:  $\tau = k_1[\text{NCl}_3]_0 t$ ,  $Y_0 = [\text{Cl}]/[\text{NCl}_3]_0$ ,  $Y_1 = [\text{Cl}_2 + 3\text{Cl}]/[\text{NCl}_3]_0$ ,  $Y_2 = [\text{NCl}_2]/[\text{NCl}_3]_0$ ,  $Y_3 = [\text{NCl}_3]/[\text{NCl}_3]_0$ ,  $\beta = k_2/k_1$ ,  $\phi = k_3/k_1$ ,  $\gamma = k_8/(k_1[\text{NCl}_3]_0)$ ,  $\lambda = k_4/(k_1[\text{NCl}_3]_0)$ ,  $\psi = k_5/k_1$ ,  $\rho = k_7/(k_1[\text{NCl}_3]_0)$ ,  $\mu = k_6/k_1$ ,  $\chi = k_9/(k_1[\text{NCl}_3]_0)$ ;  $t$  is time (s), the total pressure (Torr) is designated as  $P$ , *i.e.*,  $[\text{NCl}_3]_0 = sP$ , where  $s$  is the mole fraction of  $\text{NCl}_3$  in the initial mixture. The dimensionless velocity and coordinate of a propagating flame were defined in terms of the diffusivity of  $\text{NCl}_3$  ( $D_3$ ):  $\varpi = U/(D_3 k_1[\text{NCl}_3]_0)^{1/2}$ ,  $\xi = x/(D_3/k_1[\text{NCl}_3]_0)^{1/2}$ , where  $U$  and  $x$  are the corresponding dimensional

values. The dimensionless diffusivities ( $D_i/D_3$ ,  $i = 0\text{--}4$ )  $\delta_0$ ,  $\delta_1$ ,  $\delta_2$  in helium correspond to chlorine atoms,  $\text{Cl}_2 + 3\text{Cl}$ ,  $\text{NCl}_2$  radicals, respectively. The system of non-linear second-order differential equations for the above kinetic mechanism is the following:

$$\begin{aligned} dY_0/d\tau &= \delta_0 d^2 Y_0/d\xi^2 + 2\phi(Y_2)^2 + \psi Y_1 Y_3 + 3Y_2 Y_3 \exp(-3050/T) + \\ &\quad + 2\lambda Y_1 - Y_0 Y_3 - \gamma Y_0 \\ dY_1/d\tau &= \delta_1 d^2 Y_1/d\xi^2 + 2\phi(Y_2)^2 - \psi Y_1 Y_3 - \lambda Y_1 - \chi P Y_2 \\ dY_2/d\tau &= \delta_2 d^2 Y_2/d\xi^2 - 2\phi(Y_2)^2 + \psi Y_1 Y_3 - \rho Y_2 - Y_2 Y_3 \exp(-3050/T) \quad (\text{I}) \\ dY_3/d\tau &= d^2 Y_3/d\xi^2 - \psi Y_1 Y_3 - Y_0 Y_3 - Y_2 Y_3 \exp(-3050/T) \\ dT/d\tau &= \delta_4 d^2 T/d\xi^2 + s\beta[k_2 Y_2 Y_3 \exp(-3050/T)Q_1 + Y_0 Y_3 Q_2]/ \\ &\quad (c_p \rho) - \alpha L(T - 298)/(c_p \rho) \end{aligned}$$

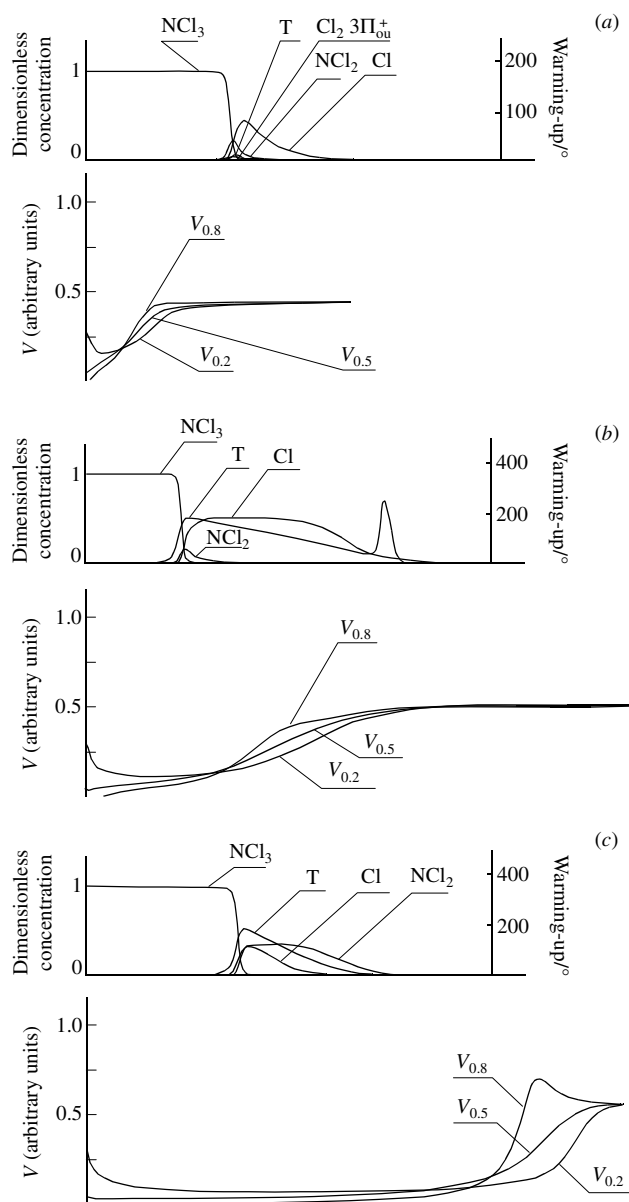
As heat evolution takes place in the chain unit, the last equation corresponds to a heat balance, where  $Q_1$  and  $Q_2$  are the specific heats,  $c_p$  is the heat capacity at a constant pressure ( $1.25 \text{ cal g}^{-1} \text{ K}^{-1}$  for He<sup>19</sup>),  $\alpha$  is the temperature conductivity,  $L$  is the surface-to-volume ratio ( $\text{cm}^{-1}$ ),  $T$  is the temperature (K),  $\alpha = L\delta e/r^2$ ,<sup>1</sup> where  $r$  is the reactor radius (cm),  $e = 2.718\ldots$ ,  $\delta$  is a critical parameter (2.0),<sup>1</sup> the thermal conductivity  $\lambda = D_{(\text{He-He})} \approx D_{(\text{He-He})}$  in dilute mixtures,<sup>28</sup>  $\delta_4 = D_{(\text{He-He})}/(D_3 c_p \rho)$ ,  $\rho$  is the density of helium ( $\text{g cm}^{-3}$ ).<sup>28</sup>

The set of equations (I) was solved numerically as described previously.<sup>16</sup> As the heterogeneous chain termination was considered to occur in a diffusive area,<sup>8</sup> the rate constants  $k_7$  and  $k_8$  were calculated by the equation  $k = 23.2D/(d^2P)$ ,<sup>3</sup> where  $d = 2r$ . The values of  $D_i$  in He ( $\text{cm}^2 \text{ s}^{-1}$ , 293 K, 760 Torr) were taken from refs. 23 and 28.

Cl	$\text{NCl}_2$	$\text{Cl}_2 + 3\text{Cl}$	$\text{NCl}_3$	He
0.73	0.44	0.55	0.41	1.62

The results of the numerical calculation of the evolution of system (I) at  $[\text{NCl}_3] = 4\%$  are shown in Figures 3(a) and 3(b) for total pressures of 5 and 35 Torr. As can be seen, the stationary velocities of flame propagation correspond to different BCR regimes: at a pressure of 5 Torr, the calculated warming-up is small ( $\sim 10^\circ$  in agreement with experimental data<sup>14</sup>) and the maximum  $[\text{Cl}_2 + 3\text{Cl}]/[\text{NCl}_3]$  ratio is as high as 0.07. It is evident that this regime of the flame propagation is practically isothermal. At a pressure of 35 Torr, the calculated value of maximum warming-up is about  $200^\circ$ ; in this case,  $[\text{Cl}_2 + 3\text{Cl}]/[\text{NCl}_3] \ll 0.07$ . The latter regime is already chain-thermal. Therefore, system (I) at  $[\text{NCl}_3] = 4\%$  admits at least two auto-wave solutions, which describe the stationary front of a propagating flame: one of them corresponds to CTFP, and the other corresponds to IFP. It was shown<sup>29</sup> that the dependence of the integral chemiluminescence intensity of  $\text{Cl}_2 + 3\text{Cl}$  on total pressure increases from 0.1 to 2 Torr (at  $[\text{NCl}_3] = 15\%$ ) and then sharply decreases with a further increase in pressure. This fact is consistent with the calculations performed [*cf.*  $\text{Cl}_2 + 3\text{Cl}$  concentrations in Figures 3(a) and 3(b)] and is evidently due to the transition from the isothermal to the chain-thermal regime of flame propagation.

The upper limit of flame propagation at 4%  $\text{NCl}_3$  is missing in experiments, as well as in calculations. It is easy to verify that two auto-wave regimes corresponding to chain-thermal and isothermal flame propagations hold for different concentrations of  $\text{NCl}_3$  at similar pressures [*cf.* Figures 2(a) and 2(b) at total pressures  $> 35$  Torr]. Actually, at  $[\text{NCl}_3] = 0.4\%$ , a chain-thermal regime of flame propagation is missing at the studied pressures in both experiments and calculations. It means that the transition to a chain-thermal regime is determined by both the initial pressure and the initial concentration of  $\text{NCl}_3$  in the mixture. The transition shows a critical character in total pressure, as is seen in Figure 2(b). IFP occurs at low pressures; an increase in the pressure causes the transition to CTFP in the pressure range (about 20 Torr) where calculated isothermal and chain-thermal solutions become separated. Note that the inclusion of heat evolution in only the linear chain branching reaction [step (2),  $Q_2 = 34 \text{ kcal mol}^{-1}$  (ref. 21)] does not cause the transition to a chain-thermal flame at pressures up to 100 Torr (Figure 2, dotted line). Therefore, the heat evolution in step (1) was also taken into account. The dependence of the calculated wave solution on the total pressure is shown in Figure 2(b) (solid line). However, a



**Figure 3** Evolution of system (I) upon calculation, 4%  $\text{NCl}_3$  in He, initial temperature of 300 K,  $Q_1 = 17 \text{ kcal mol}^{-1}$ ,  $Q_2 = 34 \text{ kcal mol}^{-1}$ . (a)  $P = 5 \text{ Torr}$ ; (b)  $P = 35 \text{ Torr}$ ; (c)  $P = 35 \text{ Torr}$ ,  $k_3$  is assumed to be zero.

wide range of parameters dealing with heat evolution ( $Q_1$ ,  $Q_2$ ,  $\alpha$ ,  $\varepsilon_i$ ) is responsible for only qualitative agreement between calculated and experimental data because the accuracy of these parameters is inadequate. Moreover, the above one-dimensional problem does not allow us to investigate the occurrence of spatial regimes inherent in BCR as non-linear dynamic systems.<sup>30</sup>

Numerical calculations allowed us to establish whether the occurrence of non-linear branching in the mechanism of BCR has an effect on the transition to a chain-thermal regime of flame propagation. For this purpose, in solving system (I) under conditions of Figure 3(b), the value of  $k_3$  was taken equal to zero, i.e., non-linear chain branching was eliminated from system (I). The results are shown in Figure 3(c). It can be seen that the transition to an auto-wave chain-thermal regime occurs within a larger time interval than that in Figure 3(a). Thus the occurrence of non-linear branching enhances the inflammability of BCR. As would be expected, an auto-wave regime is missing under conditions of Figure 3(a) (at 5 Torr): neither IFR ( $k_3 = 0$ ) nor CTFP (low warming-up) can occur. The numerical calculations can also illustrate the fact that the rate of the linear branching influences the kinetics of BCR to a greater extent than the specific heat of this reaction. Actually, the occurrence of CTFP, with  $k_3$  taken 10 times lower and with  $Q_2$  taken 10 times higher

than in previous calculations [in this case, the fifth equation of system (I), which describes heat evaluation, remains unchanged] is realized in the time interval that is four times larger than that presented in Figure 3(c).

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## References

- 1 D. A. Frank-Kamenetskii, *Diffuziya i teploperedacha v khimicheskoi kinetike* (Diffusion and Heat Transfer in Chemical Kinetics), Nauka, Moscow, 1967, p. 491 (in Russian).
- 2 V. G. Voronkov and N. N. Semenov, *Zh. Fiz. Khim.*, 1939, **13**, 1695 (in Russian).
- 3 N. N. Semenov, *O nekotorykh problemakh khimicheskoi kinetiki i reaktivnoi sposobnosti* (On Some Problems of Chemical Kinetics and Reactivity), Akad. Nauk SSSR, Moscow, 1968, p. 686 (in Russian).
- 4 V. V. Azatyan, *Kinet. Katal.*, 1999, **40**, 818 [*Kinet. Catal. (Engl. Transl.)*, 1999, **40**, 720].
- 5 V. V. Azatyan and A. A. Shavard, *Izv. Akad. Nauk, Ser. Khim.*, 1977, 2460 (*Bull. Acad. Sci. USSR, Div. Chem. Sci.*, 1977, **26**, 2279).
- 6 Ya. B. Zel'dovich, G. I. Barenblatt, V. B. Librovich and G. M. Machviladze, *Matematicheskaya teoriya goreniya i vzryva* (Mathematical Theory of Combustion and Explosion), Nauka, Moscow, 1980 (in Russian).
- 7 P. Gray, J. F. Griffiths and S. K. Scott, *Proc. Roy. Soc. Lond.*, 1985, **A397**, 21.
- 8 V. V. Azatyan, R. R. Borodulin and N. M. Rubtsov, *Fiz. Gorenia Vzryva*, 1980, **5**, 34 (in Russian).
- 9 V. P. Bulatov, V. I. Vedenev, A. N. Kitaygorodskii and O. M. Sarkisov, *Izv. Akad. Nauk SSSR, Ser. Khim.*, 1975, 1881 (*Bull. Acad. Sci. USSR, Div. Chem. Sci.*, 1975, **24**, 1763).
- 10 V. V. Azatyan, V. A. Kalkanov and A. A. Shavard, *React. Kinet. Catal. Lett.*, 1980, **15**, 367.
- 11 S. S. Nagornyi, N. M. Rubtsov, S. M. Temchin and V. V. Azatyan, in *Proc. of the Zel'dovich Memorial. International Conference on Combustion*, Moscow, 1994, vol. 2, p. 54.
- 12 F. Baillou, R. Lisbet and G. Dupre, in *Proc. of 7th Int. Symp. on Loss Prevention and Safety Promotion in the Process Industries*, Taormine, Italy, 1992, p. 43.
- 13 C. Cze, *VLSI Technology*, Wiley, New York, 1981, vol. 1, p. 905.
- 14 V. V. Azatyan, R. R. Borodulin, E. A. Markevich, N. M. Rubtsov and N. N. Semenov, *Izv. Akad. Nauk SSSR, Ser. Khim.*, 1976, 1459 (*Bull. Acad. Sci. USSR, Div. Chem. Sci.*, 1976, **25**, 1396).
- 15 N. M. Rubtsov, *Mendeleev Commun.*, 1998, 173.
- 16 N. M. Rubtsov and V. D. Kotelnik, *Mendeleev Commun.*, 2001, 61.
- 17 V. V. Azatyan, R. R. Borodulin, E. A. Markevich and N. M. Rubtsov, *Fiz. Gorenia Vzryva*, 1978, **14**, 20 (in Russian).
- 18 N. M. Rubtsov, V. V. Azatyan and R. R. Borodulin, *Izv. Akad. Nauk SSSR, Ser. Khim.*, 1980, 1234 (*Bull. Acad. Sci. USSR, Div. Chem. Sci.*, 1980, **29**, 1165).
- 19 V. V. Azatyan, R. R. Borodulin, E. A. Markevich, N. M. Rubtsov and N. N. Semenov, *Dokl. Akad. Nauk SSSR*, 1975, **224**, 1096 [*Dokl. Chem. (Engl. Transl.)*, 1975, **224**, 1059].
- 20 N. M. Rubtsov and R. R. Borodulin, in *Kinetika i mekhanizm fiziko-khimicheskikh protsessov* (Kinetics and Mechanism of Physical and Chemical Processes), Chernogolovka, 1981, p. 14 (in Russian).
- 21 T. C. Clark and M. A. A. Clyne, *Trans. Faraday Soc.*, 1970, **66**, 372.
- 22 V. V. Azatyan, R. R. Borodulin and N. M. Rubtsov, *Dokl. Akad. Nauk SSSR*, 1979, **249**, 1375 [*Dokl. Chem. (Engl. Transl.)*, 1979, **249**, 1223].
- 23 Z. I. Kaganova and B. V. Novozhilov, *Khim. Fiz.*, 1982, 1110 (in Russian).
- 24 M. A. A. Clark and H. W. Cruse, *J. Chem. Soc., Faraday Trans. 2*, 1972, **68**, 1281.
- 25 M. A. A. Clyne and D. H. Stedman, *Trans. Faraday Soc.*, 1968, **64**, 2698.
- 26 T. C. Clark and M. A. A. Clyne, *Trans. Faraday Soc.*, 1970, **66**, 372.
- 27 V. S. Posvyanski, *Skorost' i predely rasprostraneniya izotermicheskikh plamen* (Velocity and Limits of the Propagation of Nonthermal Flames), Ph. D. Thesis, Institute of Chemical Physics RAS, 1976, p. 134 (in Russian).
- 28 *Tablitsy fizicheskikh velichin* (Tables of Physical Values), ed. I. K. Kikoin, Atomizdat, Moscow, 1976, p. 1007 (in Russian).
- 29 N. M. Rubtsov, R. R. Borodulin and S. S. Saidchanov, *Khim. Fiz.*, 1984, 521 (in Russian).
- 30 G. Nicolis and I. Prigogine, *Self-organisation in Nonequilibrium Systems. From Dissipative Structures to Order through Fluctuations*, Wiley-Interscience, New York, London, Sydney, Toronto, 1977, p. 512.

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